

# Vegetable oil-derived epoxy monomers and polymer blends: A comparative study with review

R. Wang, T. P. Schuman\*

Department of Chemistry, Missouri University of Science and Technology, MO 65409 Rolla, USA

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**Abstract.** Glycidyl esters of epoxidized fatty acids derived from soybean oil (EGS) and linseed oil (EGL) have been synthesized to have higher oxirane content, more reactivity and lower viscosity than epoxidized soybean oil (ESO) or epoxidized linseed oil (ELO). The EGS and ESO, for comparison, were used neat and in blends with diglycidyl ether of bisphenol A (DGEBA). Thermosetting resins were fabricated with the epoxy monomers and either BF<sub>3</sub> catalyst or anhydride. The curing behaviors, glass transition temperatures, crosslink densities and mechanical properties were tested. The results indicated that polymer glass transition temperatures were mostly a function of oxirane content with additional influence of glycidyl versus internal oxirane reactivity, pendant chain content, and chemical structure and presence of saturated components. EGS provided better compatibility with DGEBA, improved intermolecular crosslinking and glass transition temperature, and yielded mechanically stronger polymerized materials than materials obtained using ESO. Other benefits of the EGS resin blend systems were significantly reduced viscosities compared to either DGEBA or ESO-blended DGEBA counterparts. Therefore, EGS that is derived from renewable sources has improved potential for fabrication of structural and structurally complex epoxy composites, *e.g.*, by vacuum-assisted resin transfer molding.

Keywords: thermosetting resins, mechanical properties, thermal properties, biopolymers, epoxy

### 1. Introduction

Since petroleum resources are ultimately limited, polymers based on vegetable oils are of great interest because they are renewable and could significantly contribute to a more sustainable development [1, 2]. Vegetable oils such as linseed and tung oil are drying oils, which can self-crosslink under atmospheric oxygen, have long been used in the coating industry [3]. Semi-drying oils like soybean oil are of plentiful supply and therefore of relatively low cost, have also attracted great interest for the preparation of polymers or resins [4]. In recent years, with the rising cost of fossil raw materials and environmental issues, polymers derived from soybean oil have demonstrated strong cost/performance competitiveness in many market applications [5]. However, the ability to obtain structures of sufficient mechanical or thermal properties has remained a challenge.

For instance, direct radical or cationic polymerization of vegetable oils is structurally difficult due to the non-conjugated, internal double bonds and only viscous liquid polymers with low molecular weight are formed [6]. On the other hand, polymers ranging from soft rubbers to hard plastics have been prepared by the cationic copolymerization of soybean oil blended with divinylbenzene (DVB). Styrene was added to reduce the heterogeneity of the crosslinked structures caused by incompatibility between monomers and the modulus of polymer was dependent on the styrene and, particularly, the DVB content [7].

Epoxidation of vegetable oils using peracids, such as Epoxidized soybean oil (ESO) and epoxidized

<sup>\*</sup>Corresponding author, e-mail: tschuman@mst.edu

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linseed oil (ELO), is one of the most important and useful exploitations of double bonds since epoxides are reactive intermediates that are also readily converted to other functional groups through ring-opening reactions. Sheet molding compound (SMC) resins have been made from epoxidized soybean oil modified with unsaturated functional groups like acrylic acid or maleic anhydride where styrene was employed as a comonomer to reduce the viscosity of the resin [8, 9]. The SMC was obtained via common radical polymerization fashion. Allyl alcohol ring-opened ESO has been copolymerized with maleic anhydride (MA) to prepare thermosets by esterification and free radical polymerization. The resulting glass transition temperatures  $(T_g)$  and mechanical strengths were dependent on the loading of MA [10]. Soy based polyols derived from ESO have also been widely used to produce polyurethanes that are comparable in many aspects with polyurethanes obtained from petrochemical polyols [11].

ESO can be crosslinked into thermosetting polymers by various curing agents [12]. However, due to lower oxirane content and sluggish reactivity of the internal oxirane, the cured ESO polymers normally have low crosslinking density. Poorer thermal and mechanical properties result from both partially unreacted ESO and saturated fatty acid (FA) chains that reduce reactivity and self-plasticize. Most ESO industrial uses are thus limited to nonstructural, additive applications such as plasticizers or stabilizers for poly (vinyl chloride) [13], oil-base coatings [14] with low strength requirements [15]. Though the mechanical strength of cured ESO can be improved with the addition of nano-reinforcements [16], or fiber reinforcement [17], an inherently low  $T_g$ inevitably limits practical applications because  $T_{\rm g}$ for a polymer must be appropriately higher than the temperature of its intended work environment to serve as a useful plastic [18]. When used as a matrix material in composites, the resin state is desired to be rigid/glassy, *i.e.*, below its  $T_g$ , to effectively transfer energy to fibers [19].

ESO has a moderate viscosity so ESO or their derivatives can be used as reactive diluents for the partial replacement of diglycidyl ether of bisphenol A (DGEBA) resins, which are relatively high viscosity liquids or solids, to decrease the overall cost and improve the processability [20–22]. Generally, the mechanical strengths and thermal properties of

ESO blended resins are not comparable to those of pure DGEBA epoxy resins, while their toughness can be better due to the introduction of a two phase structure [23-26]. However, due to the inhomogeneous structure, ESO is not as efficient in reducing the viscosity of epoxy resin compared to most petroleum based reactive diluents. A further increase in the ESO concentration inevitably leads to a significant decrease in performance of cured resin. There are few reports of high ESO replacement [20] because low oxirane content and the unreactive saturated component of ESO both lead to a low crosslink density upon cure and a poor miscibility exists between ESO and the DGEBA. There is an especially large difference in the reactivity of the internal oxirane in ESO and terminal oxirane in DGEBA and, as we will show, heterogeneous structures form during the curing reaction that leads to a phase separated materials of poorer mechanical /thermal performance.

More reactive terminal epoxy derived from chlorinated ESO has been reported and used as a matrix with DGEBA for glass fiber composites [27]. The dehydrochlorination under alkaline conditions will hydrolyze ester groups of triglycerides, even at room temperature. A triglyceride with terminal epoxy has been synthesized from 10-undecenoic acid and successfully used in epoxy-amine curing [28, 29], whereas 10-undecylenic acid, a derivative of castor oil, has only one terminal double bond so the epoxidized triglyceride ester of 10-undecylenic acid has a lower oxirane content compared to ESO. Largescale production also seems impractical [30]. Only those oils of poly-unsaturated FA content, especially soybean or linseed oils, that can produce dense oxirane functional resins are capable to produce satisfactory properties [12, 31-33]. Epoxidized vegetable oils (EVO) of low oxirane values either are not reactive or impart waxy, non-curing properties to the resin system.

Vegetable oils contain several actives sites amenable to chemical modification. The double bonds in FA chains and the ester groups in the glyceryl part are the most important. These active sites can be used to introduce reactive groups. ESO and aforementioned derivatives are most focused on the modification of FA chain. On the ester side, epoxidized methyl oleate [34], epoxidized methyl soyate, epoxidized allyl soyate [35], epoxidized sunflower oil biodiesel [36] and linseed oil epoxidized methyl esters [37] have been shown to have lower viscosity and more reactive compared to their ESO or ELO counterparts.

A caveat in the addition of functional groups, such as unreactive methyl or reactive allyl through transesterification, is a potential decrease of crosslinking density and final properties of cured resins upon breaking the oligomeric triglyceride structure. FA chain ends at the ester become pendant after transesterification and are dependent on crosslinking to build molecular weight. Esters of saturated FAs may only behave as plasticizers [38]. Novel epoxy compounds such as epoxidized sucrose esters of fatty acids have been synthesized and crosslinked to prepare polyester thermosets [30, 39]. High modulus polymer was achieved due to the well-defined compact macromolecular structures and high oxirane functionality. Some applications may be hampered by their high viscosities.

Modified ELO synthesized through Diels–Alder reaction of dicyclopentadiene [40] or 1,3-butadiene [41] with linseed oil have been reported. The modified ELO resins still possessed internal oxirane and thus are more suitable for cationic cure. End users still seek economical bio-based epoxies that are competitive with petroleum-based epoxies [30].

Vegetable oils generally have variable levels of saturated FA content, for example, soybean oil normally has about 15% saturated FAs (~4.0 % stearic and ~11% palmitic) that varies with plant variety, growing regions, and weather. Saturated FAs have no functional groups within the FA chain that then act as dangling chains, low in reactivity, to plasticize the final polymer. The saturated chains are detrimental to the final properties of polymers [42, 43]. To improve reactivity and to increase hydroxyl number of soy based polyols, regionally selective enzymatic hydrolysis has been attempted to liberate saturated FAs, which were then removed by alkaline washing [44]. Total removal of saturated components is difficult and is also accompanied by partial hydrolysis of unsaturated FA esters. Conversion of oil triglyceride into free fatty acid (FFA) or FA derivatives allows separation of unsaturated and saturated components on the basis of solubility through crystallization. The degree of unsaturation of FFA considerably changes the melting point and thus separation of mixtures of saturated and unsaturated FFAs can be readily achieved by proper choice of organic solvents and temperatures [45].

In this research, EGS were synthesized and examined. The goals were to remove and assess the role of the plasticizing effect of saturated components, to increase and assess the role of the oxirane content, and to minimize viscosity toward developing either a capable reactive diluent for commercial epoxy or a new commercial epoxy resin of its own right. The study gave us the opportunity to study how saturated component, oxirane type and oxirane content translate into curing, thermal and mechanical properties. We hypothesized that EGS as the ester of a terminal oxirane group (glycidyl), which is then readily accessible to nucleophilic attack, should further enable reactivity compared with the currently standard, commercial ESO and consequently reduce the molecular size and facilitate removal of the saturated FA components. We thus proposed to increase oxirane content. The goals and resin design were intended to provide a dense, intermolecular crosslinking structure and yield a more consistent thermosetting resin material with improved properties.

### 2. Experimental

### 2.1. Materials

Refined, food grade soybean oil (Great Value<sup>™</sup>, Wal-Mart, Bentonville, AR, USA) was purchased. Linseed oil was purchased from Archer Daniels Midland Company (Red Wing, MN, USA). The major FA distributions [46] reported for soybean oil and linseed oil are listed in Table 1. ESO was obtained from Union Carbide Corporation (Danbury, CT, USA). ELO was obtained from Arkema, Inc. (Philadelphia, PA, USA). Acetone, allyl alcohol, epichlorohydrin (EPCH), methylene chloride, methanol, meta-chloroperoxybenzoic acid (MCPBA), potassium hydroxide, sodium carbonate, sodium bicarbonate, sodium hydroxide, sodium sulfite, and anhy-

**Table 1.** Fatty acids profile in vegetable oils

Fatty Acid (x:y)	Palmitic (14:0)	Stearic (18:0)	Oleic (18:1)	Linoleic (18:2)	Linolenic (18:3)
Soybean oil [%]	11	4	23	53	8
Linseed oil [%]	5	4	19	15	57

Legend (*x*:*y*): *x*, number of carbon atoms; *y*, number of double bonds. Fatty acid contents do not add to 100% due to presence of minor fatty acid content.

drous sodium sulfate were purchased from Fisher Scientific (St. Louis, MO, USA). Cetyltrimethylammonium bromide (CTAB), boron trifluoride monoethyl amine complex (BF<sub>3</sub>-MEA), 2-ethyl-4-methylimidazole (EMI), hydrochloric acid and 4-methyl-1,2-cyclohexanedicarboxylic anhydride (MHHPA) were purchased from Aldrich (St. Louis, MO, USA). Commercial DGEBA was supplied by Momentive (Deer Park, TX, USA) with trade name EPON<sup>TM</sup> Resin 828. Mold release agent Chemlease<sup>®</sup> 41-90 EZ was purchased from Chem-Trend, Inc. (Howell, MI, USA)

# 2.2. Chemical characterization

Infrared spectra (IR) were measured with a Nicolet Nexus 470 E.S.P. spectrophotometer (Waltham, MA, USA). <sup>1</sup>H NMR spectra were obtained on a Varian INOVA 400 MHz spectrometer (Palo Alto, CA, USA) using  $d_6$ -DMSO as solvent. Iodine value was assessed using ASTM Method D5554-95. Oxirane oxygen value was measured using AOCS Method Cd 9-57.

# 2.3. Soap and free fatty acid preparation

Free fatty acids were made via acid neutralization of soap. Vegetable oil and water mixture (800 g, 50:50) was reacted with sodium hydroxide solution (200 g, 30 wt%) at 60°C for 4 hr to generate soap and then acidified with sulfuric acid (270 g, 30 wt%) to pH < 2. The lower aqueous layer including sodium sulfate and glycerin was separated, washing the top FFA layer using 60°C water. Finally the liquid organic FFA layer (339 g) was dried using anhydrous sodium sulfate. The iodine value of the soybean FFA was 133.

Freshly prepared FFA was dissolved in acetone based on the weight ratio of 1:6 and then purged with nitrogen gas, cooled to  $-20^{\circ}$ C for overnight. The formed crystals were removed by vacuum filtration. The procedure could be repeated several times until no further crystals were generated. For these studies, four times filtration were performed resulting in an iodine value for refined unsaturated soybean FFA of 150.

To a FFA/acetone solution (500 g) of weight ratio of 1:10, 110% of stoichiometric sodium hydroxide solution (18 mL, 10 M) based on amount of FFA (average molecular weight treated as 278 g/mol) was added dropwise. The neutralization reaction was continued for 4 hr under nitrogen gas to prevent air oxidation of the soap. The soap powder was readily filtered by vacuum filtration and then dried at 110°C for 1.5 hr.

# 2.4. Glycidyl esters of epoxidized fatty acids preparation

Dry soap (302 g) and EPCH (925 g) were heated to reflux. Phase transfer catalyst CTAB (7.3 g) at 2 equivalent-% per equivalent soap was then added. Reflux was continued for 30 min, cooled and centrifuged, the clear solution was decanted to a flask. Excess EPCH was removed using *in vacuo* rotary evaporation. Oxirane oxygen value of prepared glycidyl ester was 4.4% (theoretical value of 4.7% for glycidyl oleate).

Glycidyl ester (341 g) and sodium carbonate (64 g) were mixed with methylene chloride (200 ml). MCPBA (367 g, 75 wt%) dissolved in methylene chloride at 0.1 g/ml concentration was added dropwise at a reaction temperature below 15°C and then reacted for 4 hr to complete epoxidation. The reaction mixture was washed with 10 wt% sodium sulfite (200 g) and then by 10 wt% aqueous sodium bicarbonate (150 g). Methylene chloride was removed by in vacuo rotary evaporation and the product EGS (345 g) was dried over anhydrous sodium sulfate. Linseed oil based glycidyl esters of epoxidized fatty acids (EGL) were also prepared based on the above mentioned procedure. For EGS-S/EGL-S, saturated FFAs were not removed and remain in EGS/EGL. For EGS-P/EGL-P, FAs were partially epoxidized. Soybean oil based epoxidized methyl ester (EMS) and epoxidized allyl ester (EAS) were formed by standard alkaline transesterification with the corresponding alcohols and then epoxidized by MCPBA, e.g., potassium hydroxide (2.2 g) was first crushed and dissolved in allyl alcohol (260 g), then poured into soybean oil (220 g). Mixtures were heated under reflux condition for 4 hrs. Workup included potassium hydroxide discharged by the addition of concentrated hydrochloric acid (3.9 g, 37 wt%), removal of the excess allyl alcohol using in vacuo rotary evaporation, washing of the allyl esters of soybean oil four times with distilled water to remove glycerin, salt, and any residual allyl alcohol, and then drying with anhydrous sodium sulfate and filtration to remove the sodium sulfate. The method for epoxidation of allyl esters of soybean oil by MCPBA is the above-mentioned method for epoxidation of glycidyl esters.

# 2.5. Thermal characterization

# 2.5.1. Curing reactions

The weight ratios of EGS/ESO to DGEBA resin blend chosen for the present work were 0:100 (pure DGEBA), 10:90, 30:70, 50:50, 70:30; 90:10 and 100:0 (pure EGS/ESO). A stoichiometric ratio r =1.0 of epoxy/anhydride was used for all samples and 1 wt% (based on epoxy part) of EMI were added to the blend. After mixing by a PowerGen 1000 homogenizer (Fisher Scientific, St. Louis, MO, USA) for 10 min, the mixture was degassed under vacuum for 30 min, then poured into a mold treated with mold release agent. Curing was performed at 145°C for 15 hr for all blends except ESO-DGEBA (90:10) and pure ESO blend, which were inducted for 12 hr at room temperature, remixed, poured into the mold and cured at 125°C for 15 hr. ESO required more stringent curing conditions due to the low reactivity and phase separation exhibited by ESO. Postcure for all samples was performed at 175°C for 1 hr.

Two to three milligrams of mixture was hermetically sealed in an aluminum pan and cured on a model Q2000 differential scanning calorimetry (DSC) machine (TA Instruments, New Castle, DE, USA) by scanning temperature at a heating rate of 10°C/min from 40–250°C to study the cure behavior of each formulation.

Neat epoxy monomers were also cationically cured. A 3 wt% (based on epoxy) of BF<sub>3</sub>-MEA was mixed with monomer and cured at 150°C for 3 hr followed by 185°C for 1 hr.

# 2.5.2. Glass transition and degradation temperatures

DSC was used to determine the glass transition of cured resin. Samples were first preheated at 20°C/min to 180°C to remove any previous thermal history, and then quenched to -40°C. Heat flow was measured over a temperature range scanned from -40 to 180°C at a heating rate of 20°C/min. Universal Analysis 2000 software (TA Instruments, New Castle, DE, USA) was used to analyze the curve, inflection temperature ( $T_i$ ) was reported as the glass transition temperature.

A model Q50 thermogravimetric analysis instrument (TGA, TA Instruments, New Castle, DE, USA) was used to determine the thermal degradation onset temperature of cured resin. Measurement was performed while scanning temperature from 30 to 750°C at a heating rate of 10°C/min under an ambient air flow environment.

## 2.6. Swelling test

Approximately 0.2 g of the cured resins with a cubic shape  $(8 \text{ mm} \times 8 \text{ mm} \times 3 \text{ mm})$  were placed in toluene solvent until equilibrium was attained. To accelerate the swelling, samples were placed into a 45°C oven to attain a constant weight, then equilibrated at room temperature for one week. The swollen samples were removed from the solvents, quickly blotted dry with paper towel, and weighed. The equilibrium swelling ratio [47] of the cured resin was calculated based on Equation (1):

$$Q = \frac{1}{\nu_2} = 1 + \frac{\left(\frac{m_s}{m_0} - 1\right) \cdot \rho_{\text{poly}}}{\rho_{\text{sol}}}$$
(1)

where Q is the equilibrium swelling ratio of the polymeric network,  $v_2$  is the volume fraction of polymer at equilibrium swelling,  $m_0$  is the mass of the polymeric network before swelling,  $m_s$  is the mass of the polymeric network at equilibrium swelling, and  $\rho_{sol}$  and  $\rho_{poly}$  are the densities of the solvent and polymeric network, respectively.

### 2.7. Mechanical tests

Tensile strengths and moduli were measured on a model 4469 Universal testing machine (Instron, Norwood, MA, USA) according to ASTM D638. All the tensile tests were performed at a crosshead speed of 10 mm/min. At least five specimens were tested for each different resin system. The flexural strengths and moduli were determined according to the ASTM method D790. The span was 50.8 mm, the crosshead speed was set at 12.7 mm/min.

### 2.8. Physical properties

Viscosity was tested on a model LVDV-III+ Ultra Rheometer (Brookfield, Middleboro, MA, USA) at 25°C. Liquid density was determined using the pycnometer method. Specific gravity of solid samples was measured by immersion in water using a model XP 204S balance (Mettler-Toledo, Columbus, OH, USA) with density measurement kits.

# Results and discussion Preparation of glycidyl esters of epoxidized fatty acids

Figure 1 shows the synthetic route to EGS, generalized for oleic acid showing the process for a soybean triglyceride. Preparation of mixed FFAs from triglyceride is straightforward and well-developed. Methods of low temperature crystallization to remove the unsaturated FFAs are also well documented [48]. Most unsaturated FFAs are soluble in most organic solvents at temperature above 0°C while the saturated FFAs, which have higher melting points than unsaturated FFAs, are prone to form crystals/precipitates at low temperature in solvents like acetone or methanol. Although trace amounts of saturated FFAs remain unavoidably in the unsaturated FFAs after low temperature crystallization [49], further removal of saturated FA components was achieved after synthesis of glycidyl ester or EGS because glycidyl esters, or the epoxidized glycidyl esters, of unsaturated FAs are each liquid at room temperature and much lower in melting point than glycidyl esters of saturated FAs. The unsaturated esters are poorer solvents for saturated carbon chains, which are then more easily precipitated at room temperature. Although no FFA component analyses, like chromatography, were performed in this research, we believe the saturated components were minimized after three precipitations.

Acetone was used as a low boiling, recoverable solvent to prepare soap. A slight excess of NaOH and higher concentration was preferable when preparing soap from FFA because unsaturated FFAs were

prone to dissolve in acetone rather than react with base. Unsaturated FFA soaps are more soluble in water [50]. Carefully dried and finely powdered soaps resulted in greater yields of glycidyl esters of FAs. [51]

A low solubility of soap in EPCH suggested that a phase transfer catalyst would be useful to accelerate the reaction. With CTAB catalyst, the consumption of soap was completed within half an hour under reflux condition. Glycidyl esters can also be prepared directly from FFA in EPCH medium but the yield and purity were lower than obtained by the soap process [50]. The epoxidation of glycidyl ester was carried out using MCPBA or in situ generated performic acid. The former was more efficient. Due to the low solubility of MCPBA in methylene chlo-



Figure 2. IR spectra of (a): mixed-FFA (b): soybean oil (c): glycidyl esters (d): EGS



Figure 1. Synthetic route to EGS. (Vegetable oil and FAs are shown as simplified structures containing only oleic acid though they also contain other FAs. See Table 1)

ride, large amounts of recoverable solvent was required for the epoxidation.

Figure 2 shows the FT-IR spectra of mixed FFA, soybean oil, glycidyl esters and EGS. The band at  $3008 \text{ cm}^{-1}$  was attributed to the C–H stretching of =CH in unsaturated FAs, such as oleic acid, linoleic

acid or linolenic acid. New bands at 910 and  $852 \text{ cm}^{-1}$  were observed in the spectrum of glycidyl esters with the disappearance of the absorption at 937 cm<sup>-1</sup> in the mixed-FFA spectrum that showed presence of glycidyl group. The conversion of double bonds to epoxy was confirmed by the disappear-



Figure 3. <sup>1</sup>H NMR spectrum and structural assignments of a) FFA mixture; b) glycidyl ester of FFA mixture; and c) EGS monomer (see text for structural assignment details)

Epoxy resin	Oxirane oxygen [g/100 g sample]	EEW [g/equivalent]	Viscosity at 25°C [mPa·s]	Density [g/mL]
EGS	10.1	158	70	1.03
ESO	6.9	232	430	0.98
EGL	12.0	134	85	1.04
ELO	9.3	171	800	1.03
DGEBA	8.6	186	13 000	1.16

**Table 2.** General physical properties of epoxy resins

ance of the 3008  $\text{cm}^{-1}$  band observed in glycidyl esters and the concurrent appearance of absorption at 752  $\text{cm}^{-1}$  in EGS.

Figure 3 shows the <sup>1</sup>H NMR spectra of mixed-FFA, glycidyl ester and EGS, where linoleic acid is shown as a generalized compound for structural assignments. The spectra showed no evidence of side reactions in preparing glycidyl esters using the soap process, nearly quantitative conversion of double bonds to epoxy groups, and no oxirane ring opening during the epoxidation of glycidyl esters to EGS using MCPBA, *i.e.*, showed complete conversion but a lack of side reactions.

General properties of EGS product compared to ESO and DGEBA is shown in Table 2.

### 3.2. Curing reaction

Differential scanning calorimetry was applied to study the curing behavior of the blended epoxy resins (Figure 4). The exothermic peaks were characteristic of the epoxy and anhydride curing reaction [52, 53]. Integration of the peaks allows the determination of the enthalpy of curing reaction ( $\Delta H$ ), cure onset temperature ( $T_o$ ) and peak exothermic ( $T_p$ ).

From Figure 4, the pure DGEBA and ESO reactions with MHHPA show single exothermic reaction peak at 152°C and 216°C, respectively. The higher predominance of the  $T_p$  value of ESO means a slower reaction rate, which was also confirmed by a lower  $\Delta H$  value. A lower oxirane content of ESO and the internal oxiranes versus glycidyl functional groups react more sluggishly with MHHPA curing agent.

The addition of ESO to DGEBA leads to a shifting of  $T_p$  and  $T_o$  to higher values. With a decrease of  $\Delta H$ value, two partially convoluted peaks were clearly observed that became pronounced for 50 wt% ESO or higher ESO concentrations, which suggested that there was decreasing ESO miscibility in the DGEBA. Immiscibility would lead to an inhomogeneous cure of the epoxy resin. Group reactivity also affects the polymerization reactions. ESO has internal, hindered oxiranes whereas DGEBA has glycidyl groups of less steric hindrance and greater reactivity than the internal oxirane.

The prepared EGS resin showed quite different and interesting curing behavior. The neat EGS showed two convoluted peaks, analogous to the blend of DGEBA and ESO, which is believed to be due to the inherently different reactivity of glycidyl and internal oxirane groups. The  $T_p$  and  $T_o$  values of EGS were more than 40°C lower than ESO, which indicated EGS was much more reactive than ESO. Increased addition of EGS to DGEBA also lead to shifting of  $T_p$  to higher values but the  $T_o$  remained nearly constant. Only a 16°C increase of  $T_p$  was observed for 90 wt% EGS concentration compared to pure DGEBA while it was 54°C for a 90 wt% ESO concentration.

The  $\Delta H$ 's [J/g] also followed a similar trend. The higher oxirane content of EGS and EGS blends, which bear glycidyl groups like pure DGEBA, would appear to facilitate a more homogenous three dimensional polymer structure upon curing compared to ESO blends. Also of interest, a lower concentration of EGS/ESO, *e.g.*, 30 wt% EGS or below, or 10 wt% ESO, had little effect on the  $\Delta H$  or  $T_p$  values compared to pure DGEBA cure, which may then be related to homogeneity and compatibility with the DGEBA.

### 3.3. Compatibility

The DGEBA-ESO system generally has a heterogeneous structure [52] and, not surprisingly, a nonuniform crosslinked structure will lead to a poorer mechanical performance compared to a more homogeneous structure. Cured aromatic DGEBA polymers are much more rigid compared to cured aliphatic ESO, which behave as weak points or flaws when applying load. Fracture is initiated by the stress concentration at weak points. For instance, the mechanical properties of soybean oil/DVB plastics are significantly improved after increasing the



Figure 4. Dynamic thermograms of DGEBA-EGS/ESO-MHHPA systems

uniformity of the crosslinked structure [7]. A heterogeneous polymer structure is mainly due to the reactivity differences between internal and terminal oxirane. Moreover, the miscibility/compatibility between the monomer-monomer and monomerpolymer structures should also play an important role during the formation of crosslinked structure. Solubility parameter is one method to assess the compatibility of epoxy resin with an additive or modifie [54]. To form a homogeneous structure, the monomers and copolymers should have similar solubility parameters in accordance with the general rule that chemical and structural similarity favors solubility, *i.e.*, 'like dissolves like'. Direct determination of polymer solubility parameters from heat of vaporization data is not possible because of their non-volatility [55].

Thus, Hildebrand solubility parameters were calculated based on the group contribution method [56]. The group contribution equation is given by Equation (2):

$$\delta = \frac{\rho \sum_{i} F_{i}}{M}$$
(2)

where  $\delta$  is the calculated solubility parameter,  $\Sigma_i F_i$ is the molar attraction constant summation over discreet *i* structural group present in the compound and  $\rho$  and *M* are the density and molar mass of the compound, respectively. For polymers,  $\Sigma_i F_i$  is the sum of all the molar attraction constants in the repeat unit,  $\rho$  is the density of the polymer, and *M* is the molar mass of the repeat unit. For copolymers or polymer blends, following Equation (3) was used:

$$\delta_{\text{mix}} = \frac{\sum_{i} x_i V_i \delta_i}{\sum_{i} x_i V_i}$$
(3)

where  $x_i$  is mole fraction of component *i*,  $V_i$  is component *i* molar volume, and  $\delta_i$  is component *i* solubility parameter. In this study, the solubility parameter of each resin was calculated based on Hoy or van Krevelen model [56]. All compounds structures are listed in Figure 5. For EGS, a total 2.3 epoxy groups were used for the calculation, which was calculated from titrated oxirane content. Calculated  $\delta$  values are listed in Table 3.

From Table 3, DGEBA, MHHPA and EGS have larger solubility parameters while ESO has the lowest solubility parameter in the blend system. Calculated values of DGEBA are close to the lower limits of the experimental values [13], which are often more reliable than upper-limit ones [57]. There are some differences in the calculated values using Hoy versus van Krevelen models because epoxy group and ether group have different values in Hoy's model. Epoxy groups should convert to ether/ester after



Figure 5. Compounds structure used for solubility parameters calculation

Table 3.	Ca	lculat	ed so	olu	bi	lit	parameters	of	monomer an	d cured	l matrix

δ [MPa <sup>1/2</sup> ]	EGS	DGEBA	ESO	МННРА	DGEBA-MHHPA	EGS-MHHPA	ESO-MHHPA
$\delta$ (van Krevelen)	17.8	20.5	17.5	18.2	19.4	18.0	17.8
$\delta$ (Hoy) <sup>*</sup>	19.5 (18.6)	21.9 (21.1)	19.0 (18.4)	20.9	21.0	19.4	19.7

\*Values in brackets are calculated based on linear ether functional group instead of cyclic oxirane.

curing reaction, so values based only on ether groups instead of epoxy were also listed in Table 3. There is a considerable difference in the values of MHHPA due to the large difference between the group contributions of the anhydride group quoted by Hoy and by van Krevelen. Only van Krevelen values were used for the further calculation because there is evidence showing experimental values matched well with van Krevelen calculated values in the DGEBA-anhydride system [58].

It has been reported that ESO [59] or pre-polymerized ESO [60] is only partially miscible, *i.e.*, has phase separation, with the epoxy resins. The thermodynamic condition for polymer compatibility is that free energy change of mixing ( $\Delta G_{mix}$ ) should be small or negative, based on Flory-Huggins equation combined and Hildebrand solubility parameters [61].  $\Delta G_{mix}$  can be expressed by Equation (4):

$$\Delta G_{\text{mix}} = \phi_1 \phi_2 V (\delta_1 - \delta_2)^2 + + RTV \left( \frac{\phi_1 \rho_1}{M_1} \ln \phi_1 + \frac{\phi_2 \rho_2}{M_2} \ln \phi_2 \right)$$
(4)

where  $\phi_n$  is the phase volume fraction, V is volume of lattice,  $\rho_i$  is the density of component *i*,  $M_i$  is the molecular weight of component i, R is gas constant and T is absolute temperature. The first term of the right side in Equation (4) is related to the enthalpy of mixing  $(\Delta H_{\text{mix}})$  and the second term is assigned to the entropy of mixing  $(-T\Delta S_{\text{mix}})$ . Since  $\phi_1$  and  $\phi_2$ are fractions, for a fixed DGEBA-EGS/ESO composition,  $\Delta G_{\text{mix}}$  at constant temperature depends only on  $\Delta \delta_i$  and  $\rho_i/M_i$ , which are determined by the chemical nature and molecular weight of the EGS/ ESO/DGEBA, respectively. Proximity of  $\delta_i$  between DGEBA and EGS/ESO and a low molecular weight EGS/ESO favors the mixing process. It is not then surprising that EGS of higher solubility parameter and lower molecular weight favors better compatibility with DGEBA than ESO.

We have noticed turbid blends indicating phase separation were formed only for high contents of DGEBA replacement by ESO (90 and 100 wt%, Figure 6b, 6c and 6d), especially when using EMI as accelerator. While using tertiary amine a more transparent solution was formed but tertiary amine generally lead to lower  $T_g$  compared to using imidazole as accelerator [53]. These blends were prone to form cracked samples after curing and spots with dark brown or yellow colors were also observed



Figure 6. Physical appearances of MHHPA cured EGS/ESO-DGEBA polymers and uncured monomers blends (a): EGS-DGEBA (90:10); (b): ESO-DGEBA (90:10) precured at 145°C for 10 min; (c): ESO-DGEBA (90:10) without procuring; (d): Pure ESO inducted for 12 hrs

(Figure 6b and 6c). We ascribed these to phase separation and internal stress due to incompatibility and low reactivity of ESO in these curing systems. The terminal oxirane of DGEBA is more reactive than the internal oxirane of ESO so gelation always occurs first in the DGEBA phase. At low ESO concentration, ESO is firstly dissolved and plasticizes the rigid DGEBA matrix but is finally cured by anhydride and becomes part of the crosslinked structure as two phase thermoset polymer. At high curing temperatures, the  $\Delta G_{\text{mix}}$  is marginally negative and ESO is better compatible with DGEBA but slower to react. With the advancement of curing reaction the molecular weight of crosslinked DGEBA and ESO will increase, which will result in a decrease of  $\Delta S_{\text{mix}}$ . At a certain stage  $\Delta G_{\text{mix}}$  becomes positive and crosslinked ESO phase separates, which should be analogous to a phase separation of rubber in epoxy resin [62].

At higher ESO concentrations, due to a faster gelation rate of the glycidyl-DGEBA network occurring at low degree of conversions of ESO, internal stress can result after vitrification but which can be avoided by proper cure temperature profile [63]. Such internal stress and incompatibility can easily lead to crack initiation or defect structure as observed in Figure 6c. Prolonged induction via heated mixing of the ESO blend and carefully choosing the curing conditions led to more transparent polymers and uncracked samples that were used for further testing.

For EGS blends, due to the terminal oxirane as in DGEBA, EGS may remain part of the DGEBA matrix during curing where a more homogeneous crosslinked structure is formed. An increase in oxirane value in EGS also boosts compatibility with the DGEBA system and may yield cured products with improved properties.

#### 3.4. Crosslink density

Crosslink density is one of the most important factors determining the properties of cured thermoset resins and is typically reported as an average molecular weight ( $M_c$ ) between crosslinks. The crosslink density increases as  $M_c$  decreases. Several methods are available for measuring the crosslink density of a thermoset. A common method is to measure the elastic modulus of the thermoset in the rubbery plateau region using dynamic mechanical analysis (DMA). Solvent swelling measurements are also used to determine the crosslink density of epoxy resin [47, 64, 65]. Good agreement between  $M_c$  values from the swelling measurements based on the stoichiometry considerations has been reported [66].

A structure based on a stoichiometric curing condition was assumed because the dominant reaction in the present epoxy-anhydride-imidazole system is esterification while etherification of epoxy groups is much slower [67]. The  $M_c$  of the cured resin was calculated from equilibrium solvent swelling data

Table 4. Swelling properties of cured epoxy resins in toluene

based on the Flory–Rehner equation [47] (Equation (5)):

$$\nu = \frac{\rho_{\text{poly}}}{M_{\text{c}}} = \frac{\ln(1 - \nu_2) + \nu_2 + \chi \nu_2}{V_1 \left(\frac{\nu_2}{2} - \nu_2^{\frac{1}{3}}\right)}$$
(5)

where *v* is the strand density,  $v_2$  is the volume fraction of polymer at equilibrium swelling as measured by swelling test (Equation (1)),  $V_1$  is the molar volume of the solvent, and  $\chi$  is the polymer-solvent interaction parameter, which is related to the solubility parameters via Equation (6):

$$\chi = 0.34 + \frac{V_1}{RT} (\delta_1 - \delta_2)^2$$
(6)

where *R* is the gas constant, *T* is the absolute temperature,  $V_1$  is the molar volume of the solvent, and  $\delta_1$  and  $\delta_2$  are the solubility parameters of solvent and polymer, respectively.  $\delta_2$  was calculated by Equation (3), and where for toluene  $\delta_1 = 18.3$  MPa<sup>1/2</sup>. The calculated and experimental results are listed in Table 4.

In ESO or EGS, the epoxy crosslink sites in the FA chains are located at the 9<sup>th</sup> and 10<sup>th</sup> carbons in the oleic acid and could be also at the 12<sup>nd</sup> and 13<sup>th</sup> carbons in linoleic acid, which leave the rest of the chain up through 18<sup>th</sup> carbon as an ineffective chain end in the crosslinked polymer (Figure 7). Furthermore, the presence of saturated palmitic or stearic acids in ESO triglyceride structure also behave like pendant chain [42], so the inactive parts, *e.g.*, pendant chains and saturated FAs, in ESO and EGS constitute 34.8 and 18% of total mass, respectively. These maybe subtracted from the dry and swollen sample weights to obtain a corrected  $M_c^*$ , because

MHHPA cured	δ	ρ <sub>poly</sub>	Q	γ	M <sub>c</sub>	M <sub>c</sub> *
samples	[MPa <sup>1/2</sup> ]	[g/mL]	Swelling ratio	~	[g/mol]	[g/mol]
Pure DGEBA	19.4	1.18	1.49	0.388	257	257
EGS-DGEBA (10:90)	19.2	1.17	1.50	0.375	253	256
EGS-DGEBA (30:70)	18.9	1.16	1.54	0.356	268	278
EGS-DGEBA (50:50)	18.6	1.16	1.57	0.345	281	299
EGS-DGEBA (70:30)	18.4	1.15	1.61	0.340	304	330
EGS-DGEBA (100:0)	18.0	1.12	1.66	0.344	332	376
				•		
ESO-DGEBA (10:90)	19.3	1.17	1.51	0.375	261	267
ESO-DGEBA (30:70)	19.0	1.15	1.55	0.355	273	293
ESO-DGEBA (50:50)	18.6	1.14	1.58	0.343	285	324
ESO-DGEBA (70:30)	18.3	1.12	1.64	0.340	314	382
ESO-DGEBA (100:0)	17.8	1.09	1.84	0.350	464	640



Figure 7. Schematic representation of pendant chain in ESO structure (epoxy moieties in ESO/EGS and methane moiety in glycerol part of ESO are the crosslink sites)

end-linked networks were assumed during swelling test, in fact pendant chains are not contributed to the total crosslink densities [38].  $M_c$  and corrected  $M_c^*$  values are listed in Table 4.

From Table 4, the  $\rho$  values of both EGS and ESO systems decrease with the increase of EGS/ESO content that can be attributed to the addition of a large soft/flexible vegetable oil component to decrease the rigid, compact structure of DGEBA polymer. Increase in EGS/ESO content also leads to a higher swelling ratio Q, which could indicate not only lower crosslinking density but also a higher solubility of the network in the toluene solvent that is supported by a decreased  $\chi$  value.  $M_c$  and  $M_c^*$  values of MHHPA cured neat DGEBA [68] and neat ESO [31] are similar to reported DMA test results. Pure EGS, which has similar oxirane content as ELO, also is close to a reported DMA test result for polymerized ELO [53]. Calculated values based on the van Krevelen model are also comparable to DMA tests.

In general, an increase in ESO or EGS content decreased crosslink density compared to a neat anhydride cured DGEBA. This result is due to the inherently flexible structure of fatty acid chain and thereby prone to form a less compact crosslinked structure compared to the stiffer aromatic repeat unit of DGEBA. A decrease in crosslink density was also reported by others [20].

Crosslink density is also related to the oxirane value. EGS has higher oxirane value than ESO so all EGS blends had higher crosslink densities compared to ESO blends at the same concentration level. Crosslinking density increasing with oxirane

value has also been observed within various EVOs of different oxirane content [69] or for the same vegetable oil with different oxirane content [16]. Surprisingly, 10 wt% EGS concentration had a similar crosslink density as pure DGEBA, which is in part probably due to a higher functionality of EGS compared to pure DGEBA. More anhydride needed to cure the blend would lead to higher crosslink densities. With increases in the EGS content in blends, a lower crosslink density was observed though the crosslink density had minimal change even at 50 wt% concentration. ELO has similar epoxy content as EGS and has been reported to maintain nearly constant crosslink density of the anhydride-cured epoxy at up to 70 wt% concentration [70]. For ESO with much lower oxirane value compared to DGEBA or EGS, the crosslink density of ESO blends decreased with increased ESO concentration that is especially noticeable after  $M_c$  correction for pendant chains. The saturated component in ESO thus plays a significant role in reducing the crosslink density. Though crosslink density has been reported to not be changed by the replacement of DGEBA by ESO using mechanical analysis of the rubbery plateau [52], an artificially larger modulus can result for the inherently heterogeneous DGEBA-ESO-anhydride network due to a broadened glass transition temperature range. As heterogeneity will broaden the modulus signal in the rubbery region, a shear storage modulus value near the glass transition in the rubbery region can be artificially increased resulting in an inflated value for the calculated crosslink density.

### **3.5.** Thermal properties

The glass transition temperature  $(T_g)$  is considered a fundamental polymer characteristic related to polymer properties and processing. In general, polymers with high crosslink density have higher  $T_g$ ; however, the composition in the polymer within the crosslinked structure also plays an important role in the  $T_g$  behavior. DSC and DMA are widely used to characterize  $T_g$ . For most thermosetting plastics, the DMA measurement based on the tan  $\delta$  peak at a frequency of 1 Hz generally occurs at a temperature as much as 15–20°C above  $T_g$  as measured by dilatometry or DSC [16, 26] but inflection temperature typically correlate better with DMA tan  $\delta$  than a midpoint value.

The trend of cured epoxy resin blends (polymers)  $T_g$  as measured by DSC is shown in Figure 8. The MHHPA cured pure EGS had higher  $T_g$  (88°C) which was nearly 40°C higher than ESO-MHHPA. Pure DGEBA-MHHPA polymers which is aromatic and had the highest  $T_g$  measured (152°C). Aliphatic amine [12, 71], or boron trifluoride diethyl etherate [72, 73], cured ESO polymers had low  $T_g$ , usually less than 0°C. While aromatic amine [29], cycloaliphatic amine [74], thermally latent initiator [75], or anhydride [76] cured EVO polymers generally have higher  $T_g$ , it is still rare to observe cured ESO polymers [31, 77] with  $T_g$  above 60°C.

Addition of ESO or EGS led to a decrease of  $T_g$ . For small EGS/ESO concentration, *e.g.*, below 30 wt%, the  $T_g$  values of ESO-DGEBA or EGS-DGEBA systems were quite similar to each other and slightly decreased compared to pure DGEBA-MHHPA, which indicated the  $T_g$  behavior was mainly determined by the crosslink density as measured in the swelling test where only slight increases of  $M_c$  or  $M_c^*$  were observed. However, the aromatic DGEBA versus aliphatic EGS structure also plays a role because 10 wt% EGS concentration appears to have a slightly higher crosslink density but still a lower  $T_g$ . It has been reported that aromatic phthalic anhydride cured EVO had higher  $T_g$  but lower crosslink density [31, 53].

For further increases in the concentration of EGS/ ESO, the  $T_g$  values decreased more rapidly, especially for the ESO system. The inherent, long aliphatic chain structure of ESO, sluggish reactivity of internal oxirane, and lower oxirane content preclude polymer as densely crosslinked as those of EGS or DGEBA. Unreactive saturated components like stearic acid and palmitic acid pendant chains enhance the flexibility and degree of freedom for movements of the molecular chains in the epoxy network. These factors decrease the polymer  $T_g$ . Further depressed  $T_g$  was also reported for an epoxidized palm oil system, which had lower oxirane content than ESO [26].

At low ESO concentrations ( $\leq$ 50 wt%) a linear, decreasing  $T_g$  trend was observed, however, neat ESO or higher ESO concentrations ( $\geq$ 50 wt%) thermosetting polymers showed broad transitions from the glassy to the rubbery state. The blends'  $T_g$  seems predominately controlled by the ESO part. Similar behavior was also found in ELO replacement of diglycidyl ether of bisphenol F resin [78]. The plasticizing effect of saturated FAs and/or the different reactivity of ESO and DGEBA leads to a broad distribution of chain segment mobilities [79] and indicate a heterogeneous polymer network [80]. Broad  $T_g$  range behavior was not found in the EGS-DGEBA systems. Also a nearly linear transition of  $T_g$  with increase of EGS was observed, which indi-



**Figure 8.** Plots of a) the glass transition region of ESO/EGS-MHHPA neat polymer showing the differences in breadth of the transition; b) the measured inflection point glass transition temperatures of cured epoxy monomer(s) as a function of ESO/EGS-DGEBA blend composition (Lines only to aid visualization of trend)



Figure 9. Polymer glass transition temperatures as a function of monomer oxirane contents through cationic homopolymerization and MHHPA copolymerization. [Note: straight lines are to indicate trend; vertical bars indicate the breadth of glass transition region equal to the difference between onset temperature and endset temperature as determined in DSC].

cated good synergy and homogeneity of the crosslink structure formation between EGS and DGEBA.

Researchers [16, 69] have noted the influence of EVO monomer oxirane value on polymer  $T_g$ . We present trends in relationship between  $T_g$  and EVO structure with and without saturated components. Several epoxy resins made from vegetable oils were synthesized and polymerized by MHHPA with EMI as catalyst and/or cationically polymerized with BF<sub>3</sub>-MEA initiation. The obtained plot of polymer  $T_g$  as a function of oxirane oxygen value is presented in Figure 9.

The glass transition temperatures of anhydride cured copolymers are higher than those of the neat of cationically cured monomers due to the anhydride structural stiffness elevating the copolymer  $T_g$ . The  $T_g$  are observed to increase fairly linearly with oxirane value. Higher oxirane values are expected to lead to higher crosslink densities upon curing. A similar  $T_g$  for anhydride cured ELO and EGS was observed though ELO has a slightly lower oxirane value. The ELO structure is partially crosslinked, *i.e.*, glycerol crosslinks the three FFAs, and would have a slightly higher oxirane value if converted to the glycidyl structure like EGS. Linseed oil is also richer in linolenic acid content that may facilitate a dense crosslinked structure.

EGS and EGL have much higher  $T_g$  compared to their respectively ESO or ELO counterparts. A  $T_g$ value of 124°C was measured for EGL, which appears unprecedented for a vegetable oil based thermoset polymer. The  $T_g$  increases in EGS-S/ EGS-P and EGL-S/EGL-P are mainly due to the addition of the reactive glycidyl group compared to ESO and ELO. Removal of the saturated components greatly increases the  $T_g$ . A 30 and 20°C increase in polymer  $T_g$  was observed for MHHPA cured EGS and EGL compared to EGS-S and EGL-S, respectively. Such trends are observed in the  $M_c$  calculations as a significant increase of crosslink density upon exclusion of the saturated components.

Adding an unreactive function group, e.g., allyl (EAS) or methyl groups (EMS), generates a lower  $T_{\rm g}$  though the oxirane values are similar to that of ESO. Since the allyl group in EAS is partially epoxidized, EAS has even slightly higher oxirane value than ESO. The  $T_{g}$ 's are greatly decreased compared to ESO because, unlike ESO that is partially crosslinked through glycerol, transesterification engenders all the fatty acid carbons except carbons in the epoxy groups into pendant chains. In addition, the liberated saturated FFA esters behave as plasticizers in the matrix to increase the chain segment mobility and decrease crosslink density. Monofunctional epoxidized methyl oleate and epoxidized oleic acid have lower oxirane content compared to EMS and were difficult to polymerize by our current curing conditions though polymer  $T_{\rm g}$  of -14 to -50°C have been reported [36, 81].

Broader  $T_{\rm g}$  regions (onset-endset ranges are provided in Figure 9 using bars; NOTE: the vertical bars are not 'error' bars or deviations but indicate the measured temperature range breadth of the glass transition) indicate a broader distribution of chain environments and heterogeneous structures were observed in anhydride cured ELO and ESO. We ascribe the less homogenous polymer structures to a low reactivity of internal oxirane in ELO or ESO instead of saturated components because even EGS-S and EGL-S with saturated FFAs show relatively sharp glass transition ranges. Indeed, internal epoxy is more reactive in cationic polymerization where all epoxies show a similar transition breadth when initiated by BF<sub>3</sub>-MEA. EMS of all internal oxirane structure and saturated FFA also show a narrow glass transition region, which could be due



Figure 10. TGA of MHHPA cured EGS-DGEBA blends compared to pure EGS and pure DGEBA

to greater reactivity of the small molecules during curing compared to large oligomers of ESO or ELO [37].

Figure 10 presents the TGA weigh loss as a function of temperature curves for the polymerized epoxy resin. Since the ESO-DGEBA blend had a similar thermal stability as the EGS-DGEBA blend, only the latter is shown here. TGA results indicated all cured EGS-DGEBA resins appear thermally stable to temperatures at least 300°C. Replacements of DGEBA by EGS led to an earlier onset of degradation. All epoxies presented two stage degradation behavior. The first stage of decomposition from 300 to 450°C is believed to be due to decomposition of unreacted MHHPA, dehydration of hydroxyl groups, and the pyrolysis of the crosslinked epoxy resin network. The second stage loss from ~450 to 600°C was considered to be the complete decomposition of the smaller fragments like cyclized or aromatic degradation byproducts as indicated by the decrease of char residue when EGS component was increased.

#### 3.6. Mechanical performance

Flexural and tensile properties of the polymerized resin systems as a function of ESO/EGS content were determined. The results are shown in Figures 11 and 12. Smaller concentrations of EGS led to only minor changes in strength or modulus compared to neat DGEBA. An improvement in flexural modulus was observed for 10 wt% EGS. Similar results, showing improved modulus at low replacement concentrations, have also been reported for an amine cured, soy-based epoxy resin system [35]. These data correlate with minor changes of  $M_c$  cal-



Figure 11. Tensile and flexural strengths of MHHPA and EGS/ESO-DGEBA blend copolymerization products



Figure 12. Tensile and flexural moduli of MHHPA and EGS/ ESO-DGEBA blends copolymerization products

culated at low concentrations of EGS/ESO in DGEBA system blends.

However, the modulus and strength values of the blends systematically decreased with further increases in ESO/EGS concentration. These phenomena are readily explained by a decrease of stiffer, bulky aromatic group content and a decreased crosslinking density of the cured blends. All the EGS-DGEBA blends showed higher strength and modulus than the ESO-DGEBA blends of comparable concentration, which is supported by smaller  $M_{\rm c}$ or  $M_c^*$  of EGS compared to ESO. The flexural stress and modulus of EGS-DGEBA exhibited a gradual decrease until 50 wt% followed by a more abrupt change. For ESO-DGEBA, large materials property losses occurred at  $\geq$  30 wt%. The study of ref [35] studied compositions only up to 30 wt% soy epoxy resin. Similarly, the tensile strength of EGS-DGEBA

had only minor changes up to 70 wt% concentration whereas a continuous decrease in strength was observed for ESO-DGEBA blends. As observed in Figures 4 and 6, EGS was observed to be more reactive and compatible with DGEBA and a higher content of EGS was achieved with greater homogeneity than comparable ESO blends and greater mechanical strengths.

### 3.7. Viscosity reducing ability

Reactive diluents are used for reducing and controlling the viscosity of epoxy resins to improve wetting and handling characteristics because in the liquid-molding technologies like resin transfer molding or pultrusion, the viscosity and resin flow are critical to achieving a quality laminate [82]. Recent trends toward lower volatile organic compounds (VOC), higher solids epoxy formulations have also resulted in increased utilization of reactive diluents [83]. It was found that EGS had inherently lower viscosity than ESO. EGS has an extra glycidyl group and lower molecular weight compared to ESO, which is a triglyceride and has oligomeric behavior. The viscosity reducing abilities of EGS and ESO were compared at different concentrations of replacement of the DGEBA resin, which had a relatively high viscosity of 13 000 mPa·s (see Figure 13). ESO and EGS have different miscibility with DGEBA resin; however, EGS exhibited a much better viscosity reducing efficiency than ESO. A 30 wt% concentration of EGS reduced the DGEBA resin viscosity to value below 1000 mPa·s, which is indispensable for many applications. At



Figure 13. Viscosity of DGEBA blended with various EGS or ESO concentrations

least 50 wt% of ESO was needed to reduce DGEBA resin to 1000 mPa·s viscosity.

### 4. Conclusions

Bio-based epoxy resins, glycidyl ester of epoxidized fatty acids, were produced from soybean or linseed oils with a reduced saturated FFA fraction content. The products were characterized and showed high oxirane contents that were more reactive than ESO or ELO, which was shown to directly impact polymer homogeneity and glass transition temperature. Epoxy monomers from other vegetable oil sources such as canola, palm, corn, *etc.*, could be fabricated in similar fashion and have similar properties and curing behaviors providing that saturated fatty ester chains are similarly removed.

The vegetable oil based epoxy resins displayed glass transitions that appear to be mostly a function of oxirane content but with additional influences of glycidyl versus internal oxirane reactivity, pendant chain content, and chemical structure and presence of saturated components. Generally, higher oxirane contents (epoxy functionality) lead to higher glass transition temperatures whereas reduced epoxy functionality, non-glycidyl FFA esters, and greater pendant chain contents lead to lower glass transition temperatures. In blends with DGEBA, monomers with only less reactive internal epoxies led to a more heterogeneous polymer structure compared to monomers possessing the more reactive glycidyl group and improved polymer homogeneity, in cure and structure. The inherent, long chain aliphatic structure of these thermoset monomers limits polymer glass transition temperatures compared to commercial, aromatic based epoxy monomers (DGEBA) but our data provide a clear trend and role of oxirane content.

The EGS blends with DGEBA were cured by MHHPA and their thermosetting polymer  $T_g$ 's measured in comparison to control ESO blends with DGEBA, which were polymerized in similar fashion. The EGS polymers displayed improved  $T_g$ 's and mechanical properties compared to their ESO counterparts and, in addition to an inherently low viscosity and efficient viscosity reduction, should therefore be more attractive as a reactive diluent. For instance, EGS derived from renewable sources could further enable defect-free fabrication of complex, shaped epoxy composites for structural com-

posite applications. Our data show ESO produced less homogeneous polymers when blended with DGEBA epoxy that resulted in thermal cure, thermal property, and mechanically inferior materials compared to the more compatible EGS epoxy resin and blends. The compatibility and superior properties arise from the removal of saturated pendant chains, addition of the glycidyl structure, and larger internal oxirane content inherent of EGS.

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### Abbreviations

DGEBA	diglycidyl ether of bisphenol A
EAS	epoxidized allyl ester of soybean oil
EMI	2-ethyl-4-methylimidazole
EMS	epoxidized methyl ester of soybean oil
EPCH	epichlorohydrin
EGL	glycidyl esters of epoxidized fatty acids derived
	from linseed oil
EGL-P	EGL with partially epoxidized fatty acids
EGL-S	EGL included saturated fatty acids
EGS	glycidyl esters of epoxidized fatty acids derived
	from soybean oil
EGS-P	EGS with partially epoxidized fatty acids
EGS-S	EGS with saturated fatty acids
ELO	epoxidized linseed oil
ESO	epoxidized soybean oil
EVO	epoxidized vegetable oils
FA	fatty acid
FFA	free fatty acid
MCPBA	meta-chloroperoxybenzoic acid
MHHPA	4-methyl-1,2-cyclohexanedicarboxylic anhydride

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